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MECHANISM OF THE OXIDATION OF PROPENE

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[Tables referred to are appended.]

In 1949, we published [1] quantitative results of chemical research into high-temperature and low-temperature oxidation of the mixture  $C_3H_6 + O_2$ . On the basis of these data, we tried to add up the balance of C,  $H_2$ , and  $O_2$  through the entire course of the reaction. As seen in Table 1, the balance adds up with sufficient accuracy. Here it is apparent that over the entire run of the reaction, the amount of water obtained (the only product not determined by analysis but by difference from the balance) is equal to the sum of CO and  $CO_2$ . In low-temperature oxidation (see Table 2) there is a disparity between the amount of carbon burned and that found in the reaction products, a disparity which increases with the extent of the transformation. This amount of carbon escaping analysis is explained as due to the polymerization of formaldehyde which takes place during low temperature oxidation. Its calculation leads to the same agreement between the quantities of water and the sum of CO and  $CO_2$  which was noted for the high-temperature reaction.

Comparison of the results of low- and high-temperature oxidation of propene leads to the conclusion, as was shown previously [1], that there is a significant resemblance between processes in both temperature ranges. Apart from what was said in the previous report, a very important argument supporting this is the fact that at both temperature ranges, identical quantities of oxygen are consumed for the same amount of converted propene throughout the course of the reaction.

- 1 -

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Supporting points on which the scheme is based are as follows:

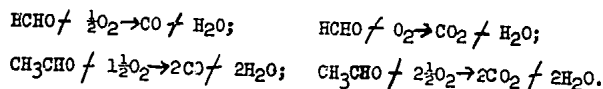
1. The close similarity of chemical processes established for high- and low-temperature oxidation is a reflection of the same radical-chain mechanism for both temperature ranges.

Low-temperature flashing is not reflected in this scheme, being a side process of no significance in the total reaction of oxidation.

2. Over its entire extent, the process of oxidation of propene leads to the conversion of this substance into  $C_2H_4$ , HCHO,  $CH_3CHO$  and subsequent oxidation of the aldehydes, into CO,  $CO_2$ , and  $H_2O$ .

3. HCHO formed in the reaction is not a degradation product of  $CH_3CHO$ . As was shown by special experiments, addition of  $CH_3CHO$  to the original propene-oxygen mixture does not increase the yield of HCHO.

4. Further oxidation of the aldehydes proceeds according to the following over-all equations:



5. The sum of the quantities of CO and  $CO_2$  formed is equal over the entire run of the reaction to the amount of water formed.

6.  $CH_3CHO$  brings about the degenerate-branched character of the oxidation.

#### Scheme of the Oxidation

- |  |   |
|--|---|
| 1. $C_3H_6 + O_2 \rightarrow \dot{C}_3H_5 + HO_2$              | 6. $HCO + C_3H_6 \rightarrow HCHO + \dot{C}_3H_5$             |
| 2. $\dot{C}_3H_5 + O_2 \rightarrow C_3H_5OO\dot{O}$            | 7. $\dot{C}H=CH_2 + C_3H_6 \rightarrow C_2H_4 + \dot{C}_3H_5$ |
| 3. $C_3H_5OO\dot{O} \rightarrow HCHO + \dot{C}H_2CHO$          | 8. $CH_3CHO + O_2 \rightarrow \dot{C}H_2CHO + HO_2$           |
| 4. $\dot{C}H_2CHO + C_3H_6 \rightarrow \dot{C}_3H_5 + CH_3CHO$ | 9. $2HCHO + O_2 \rightarrow \text{end products}$              |
| 5. $C_3H_5OO\dot{O} \rightarrow H_2O + CO + \dot{C}H=CH_2$     | 10. $2CH_3CHO + O_2 \rightarrow \text{end products}$          |
| 6. $\dot{C}H=CH_2 + O_2 \rightarrow HCHO + HCO$                | 11. $C_3H_5OO\dot{O} \rightarrow \text{breaking away}$        |

In the beginning stages of the oxidation of  $C_3H_6$ , when only traces of CO and  $CO_2$  are detected, it may be assumed that practically the entire amount of aldehydes is covered by the analysis. In high-temperature oxidation of propene, 165 seconds after the introduction of the mixture into the reaction vessel, the following were found: HCHO, 4.03 mm;  $CH_3CHO$ , 2.3 mm;  $C_2H_4$ , 0.7 mm, and traces of CO and  $CO_2$ . In low-temperature oxidation of propene, 25 minutes after introduction of the mixture into the reaction vessel, the following were found: HCHO, 7.1 mm,  $CH_3CHO$ , 3.9 mm,  $C_2H_4$ , 1.2 mm, and traces of CO and  $CO_2$ . From this, it follows that in the beginning stages of the reaction, (a) the ratio of the actually formed quantities of HCHO to  $CH_3CHO$  is close to 2; and (b) the ratio of the quantity of formed  $C_2H_4$  to the actually formed quantity of HCHO is close to 1/5.

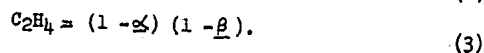
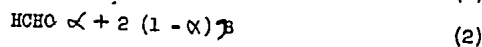
Taking the rate of the first reaction of the scheme to be 1, the rate of the second will be  $\alpha$ , of the fourth 1 -  $\alpha$ , of the fifth (1 -  $\alpha$ ) $\beta$  and of the seventh (1 -  $\alpha$ )(1 -  $\beta$ ), where  $\alpha < 1$  and  $\beta < 1$ . Using these designations, we get for the quantities of actually formed products (i.e., without considering their further oxidation):

- 2 -

CONFIDENTIAL

CONFIDENTIAL

50X1-HUM



Then, for the beginning stages of the reaction,

$$\frac{\text{HCHO}}{\text{CH}_3\text{CHO}} = \frac{\alpha + 2(1 - \alpha)\beta}{\alpha} = 2$$

$$\frac{\text{C}_2\text{H}_4}{\text{HCHO}} = \frac{(1 - \alpha)(1 - \beta)}{\alpha + 2(1 - \alpha)\beta} = \frac{1}{5}$$

whence  $\alpha = 0.525$  and  $\beta = 0.55$ .

Since  $\alpha$  determines the relationship of two monomolecular processes with the same radical  $\text{C}_3\text{H}_5\text{O}$  (reactions 2 and 4), it remains constant throughout the reaction.

From the scheme, we get

$$\beta = \frac{k_5(\text{C}_2\text{H}_3)(\text{O}_2)}{k_5(\text{C}_2\text{H}_3)(\text{O}_2) + k_7(\text{C}_2\text{H}_3)(\text{C}_3\text{H}_6)} = \frac{1}{1 + \frac{k_7(\text{C}_3\text{H}_6)}{k_5(\text{O}_2)}} \quad (4)$$

Thus, the value of  $\beta$  depends on the ratio  $(\text{C}_3\text{H}_6)/(\text{O}_2)$ , which changes from 1.02 to 4.57 and from 1.1 to 6.6 at the end of the reaction in the high- and low-temperature regions, respectively.

Substituting the values for  $\beta$ ,  $\text{C}_2\text{H}_4$ , and  $\text{O}_2$  in equation 4 for the moment of the reaction which corresponds to 165<sup>3</sup> seconds for the high-temperature regions and 25 minutes for the low-temperature regions, we find the relation of  $k_7/k_5$ . From the analytical data on  $(\text{C}_3\text{H}_6)/(\text{O}_2)$  during the course of the process and the relation of  $k_7/k_5$ ,  $\beta$  is determined for any moment of the reaction.

Knowing  $\alpha$ ,  $\beta$ , and the amount of consumed propene, it is possible to determine the actual amounts of formaldehyde and acetaldehyde by using equation 1 and 2. Deducting from them the analytically determined amounts of aldehydes, we find the quantity of aldehydes subjected to oxidation, i.e., the amount of CO and  $\text{CO}_2$  formed. Furthermore, CO, obtained by reaction 4, is determined as the sum

$$\frac{1}{2}[\text{HCHO}_{\text{initial}} - (\text{CH}_3\text{CHO})_{\text{initial}}] + (\text{C}_2\text{H}_4).$$

Table 3 contains the results of calculations of this type for the high- and low-temperature regions. As we can see, the calculated amounts of CO correspond well to the analytically determined quantities of CO +  $\text{CO}_2$ , which is a confirmation of the proposed chain mechanism.

[Appended tables follow.]

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Table 1. Balance in mm of C, O<sub>2</sub>, and H<sub>2</sub> Along the Course of High-Temperature Oxidation of the Mixture C<sub>3</sub>H<sub>6</sub> + O<sub>2</sub> (T = 3700; P initial = 220 mm, t\* 2 min 35 sec)

Moment of Reaction in sec After Introduction of Mixture to Reaction Vessel	C			O <sub>2</sub>			H <sub>2</sub>			CO/CO <sub>2</sub>
	Consumed	Found in Formed Substances	Remainder	Consumed	Found in Formed Substances	Remainder	Consumed	Found in Formed Substances	Remainder	
190	57	52.5	4.5	32.5	23.55	8.95	57	35.5	21.5	17.2
191.5	61.5	57.25	4.25	35	25.4	9.6	61.5	39	22.5	18.9
195	98.1	92.9	5.2	56	41.6	14.4	98.1	65.4	32.7	28.7
197.5	105	102.3	2.7	62	45.8	16.2	105	70.4	34.6	33
202	120	114	6	75	49.7	25.3	120	73.7	46.3	41
207.5	135	135.9	-	89.6	59.4	30.2	135	80.5	54.5	53.4
215	153	146.6	6.4	95.5	64.5	31	153	83.5	69.5	63.1

/ \* Induction period

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50X1-HUM

Table 2. Balance in mm of C, O<sub>2</sub>, and H<sub>2</sub> Along the Course of Low-Temperature Oxidation of the Mixture C<sub>3</sub>H<sub>6</sub> + O<sub>2</sub>  
(T = 300°; P<sub>initial</sub> = 320 mm,  $\bar{t}$  = 30 min 45.6 sec) (case of three cold flames)

Moment of the Reaction	C					O <sub>2</sub>			
	Con- sumed	Found in Sub- stances	Differ- ence	Spent in Polymeri- zation	Remainder After Cal- culation of Polymer- ization	Con- sumed	Found in Sub- stances	Spent in Polymeri- zation	Remain- der
30 min 40.5 sec	72	67.2	4.8	3	1.8	43	30.5	1.5	11.0
End of $\bar{t}$ (before first cold flame)	93	85.8	7.2	4.8	2.4	53	37.6	2.4	13.0
End of first cold flame	105	97.1	7.9	5.2	2.7	62.5	44	2.6	15.9
Before second cold flame	111	100	11	8.2	2.8	68.5	45	4.1	19.4
End of second cold flame	126	109.7	16.3	12.8	3.5	78	49.3	6.4	22.3
Before third cold flame	144	118.7	25.3	21.5	3.8	91.5	54.75	10.75	26
End of third cold flame	171	131.5	39.5	35	4.5	110.5	60.75	17.5	32.25
End of reaction	213	168.6	44.4	39	5.4	144	82.13	19.5	42.37

CONFIDENTIAL

- 5 -

[Adjoins page 6 here.]

CONFIDENTIAL

50X1-HUM

H<sub>2</sub>

<u>Consumed</u>	<u>Found in Formed Substances</u>	<u>Spent in Polymerization</u>	<u>Remainder</u>	<u>CO + CO<sub>2</sub></u>
72	46.05	3	23	21.9
93	61.4	4.8	26.8	25.4
105	64.5	5.2	35.3	33.7
111	62.8	8.2	40	38.3
126	65.7	12.8	47.5	44.8
144	69.1	21.5	53.4	50.7
171	67.5	35	68.5	63
213	75.5	39	98.5	93.4

CONFIDENTIAL

- 6 -

[Adjoints page 5 here.]

CONFIDENTIAL

50X1-HUM

Table 3. Comparison of Quantities of (CO + CO<sub>2</sub>) Calculated According to the Scheme With Quantities Found Analytically in the Course of Oxidation of the Mixture C<sub>3</sub>H<sub>6</sub> + O<sub>2</sub>  
(quantities of substances in mm)

Moment of the Reaction	B*	C <sub>3</sub> H <sub>6</sub> O <sub>2</sub>	C <sub>3</sub> H <sub>6</sub> Ini- tial	Analytically Found		Actually Formed		HCHO, Lost in Poly- merization	CO + CO <sub>2</sub>		
				CH <sub>3</sub> CHO	HCHO	C <sub>2</sub> H <sub>4</sub>	CH <sub>3</sub> CHO		HCHO	Calculated From Scheme	Analyti- cally Found
High-Temperature Region (T = 3700°; P <sub>initial</sub> = 220 mm α = 0.525)											
165 sec	0.55	1.02	3.5	2.3	4.03	0.7	--	--	--	--	--
190 "	0.515	1.18	19.0	7.1	12	3.0	10.0	20.1	--	21.9	17.2
191.5 "	0.511	1.2	20.5	7.1	14.85	3.5	10.75	21.6	--	21.2	18.9
195 "	0.463	1.45	32.7	12.3	25.6	4.8	17.2	33.5	--	30.6	28.7
197.5 "	0.422	1.59	35	12.5	27.2	6	18.4	35.7	--	35	33
202 "	0.378	2.06	40	12.3	28	8	21.0	40.2	--	47.2	41
207.5 "	0.268	3.46	45	13	28.5	10	23.6	44.35	--	57.3	53.4
215 "	0.214	4.57	51	13.5	28.8	10.7	26.7	46.4	--	68.1	63.1
Cold-Flame Region (T = 3000°; P <sub>initial</sub> = 320 mm; α = 0.525)											
30 min 16.5 sec	0.545	1.1	19	6.0	14.1	2.5	9.95	19.6	--	--	--
30 min 16.5 sec	0.53	1.16	24	9	19	3.75	12.6	24.7	3.0	19.8	21.9
End of τ**	0.52	1.21	31	12	25	4.8	16.2	32.0	4.8	23.3	25.4
End of first cold flame	0.505	1.29	35	12.3	26	5.3	18.3	36.0	5.2	30.9	33.7

[Adjoins page 8 here.]

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50X1-HUM

[Adjoins page 7 here.]

Before second cold flame	0.49	1.35	37	10.5	24	7.2	19.4	38	8.2	40.1	38.3
End of second cold flame	0.475	1.46	42	11.1	24.6	7.9	22	42.9	12.8	45.6	44.8
Before third cold flame	0.44	1.67	48	11.6	25.5	8.3	25.5	48.6	21.5	48.8	50.7
End of third cold flame	0.38	2.15	57	11.0	24.0	9.0	30	56.9	35	60.5	63
End of reaction	0.167	6.6	71	12.3	27.4	9.8	37.2	67.8	39	76.3	93.4

\*For calculating the actual quantities of HCHO, we made use of the average value of  $\bar{E}$  for every moment of the reaction

\*\*End of induction period, i.e., moment of origination of first cold flame

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1. V. Ya. Shtern and S. S. Polyak, DAN SSSR, Vol LXV, No 3, 311 (1949)
2. V. Ya. Shtern and S. S. Polyak, DAN SSSR, Vol LXVI, No 2, 235 (1949)

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- 8 -  
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50X1-HUM